Invariant Observer Applied to Anaerobic Digestion Model

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Abstract—In this note, we design an invariant observer for a two step (acidogenesis-methanogenesis) mass balance non linear model, in order to estimate simultaneously all bacteria and substrate concentrations found in the anaerobic digestion process. The particularity of the designed observer is the use of only the methane flow rate which is cheap to measure and commonly measured online even at industrial scale.

Index Terms—Non-Linear Models; Invariant Observer; Anaerobic Digestion.

I. INTRODUCTION

The Anaerobic Digestion (AD) is a promising process for waste valorisation and energy production. It consists on the transformation of organic matter into biogas, which is a mixture of gaseous, through several biologic reactions including different species of microorganisms. The produced biogas is then converted to electrical energy and injected to the power grid. Despite the advantages that can present the AD process, it has still not found its place in industry due to the lack of process knowledge. In fact, this goes back to the lack of sensors and the expensive price of the existing ones. To overcome this issue, a couple of software sensors has been designed. Among them, we can cite the asymptotic observer reported in [2] which is quite simple and does not require the knowledge of some specific non linear functions. However, it has a drawback concerning the speed of convergence which is equal to the control input. An extension of the asymptotic observers has been proposed in [3] which has the advantage of using reliable measurement, which are non linear functions of the state vector, to improve its estimation. The same authors have proposed interval observers to estimate the interval where the state is lying when the system has large uncertainties. However, generally the rate of convergence is not tunable. A new kind of observers has been proposed in [1] and [8] and applied to a class on chemical reactors, they are called invariant observers and are based on Lie group symmetries. The advantage of such observers is their adjustable and robust convergence as it has been shown in [5]. In the present work, we apply an invariant observer to a non linear model for the AD process with the only use of methane flow rate measurement, which is cheap and easy to do online. The present note is organised as the following: In Sec. (II) we present the studied model, then in Sec. (III) we give brief notions about the invariant observer and the needed ingredients to design it. In Sec. (IV) we detail the designed observer and give the prove of convergence. Finally, after showing the simulation results in Sec. (V) we conclude the paper in Sec. (VI).

II. MODEL DESCRIPTION

The nonlinear model for the AD process reported in [6] considers the following two reactions as the limiting steps:

1) Acidogenesis with reaction rate $r_1 = \mu_1 x_1$:

$$\begin{align*}
k_1 s_1 \rightarrow x_1 + k_2 s_2 + k_4 c_2 
\end{align*}$$

2) Methanogenesis with reaction rate $r_2 = \mu_2 x_2$:

$$\begin{align*}
k_3 s_2 \rightarrow x_2 + k_5 c_2 + k_6 c_4 
\end{align*}$$

where, $s_1$ ($Kg/m^3$) is the organic substrate degraded by the acidogenic bacteria $x_1$ ($Kg/m^3$) to volatile fatty acids $s_2$ ($mol/m^3$) which are supposed to behave like pure acetate, and $x_2$ ($Kg/m^3$) is the methanogenic bacteria which consume $s_2$ and produce $c_2$ and $c_4$. The substrates and microorganisms concentrations are modelled by the following equations:

$$\begin{align*}
s_1 &= D(t)(s_{1in} - s_1) - k_3 \mu_1(s_1)x_1 \\
x_1 &= (\mu_1(s_1) - \alpha D(t))x_1 \\
s_2 &= D(t)(s_{2in} - s_2) + k_2 \mu_1(s_1)x_1 - k_3 \mu_2(s_2)x_2 \\
x_2 &= (\mu_2(s_2) - \alpha D(t))x_2
\end{align*}$$

with:

$$\begin{align*}
\mu_1(s_1) &= \mu_{1max} s_1 \frac{x_1 + k_{s1}}{s_2 + k_{s1} + x_1} \\
\mu_2(s_2) &= \mu_{2max} s_2 \frac{x_2}{s_2 + k_{s2} + x_2}
\end{align*}$$

where, $s_{1in}$ and $s_{2in}$ are the input concentrations of $s_1$ and $s_2$ respectively, $D\left(\frac{1}{day}\right) > 0$ is the dilution rate and is the control variable, $k_i$ are the yield coefficients defined in Table (I) with the other parameters. In this work we take $\alpha = 1$ which corresponds to an ideal Continuous Stirred Tank Reactor (CSTR) [6], and we choose the output to be the methane gas flow rate:

$$\begin{align*}
y = k_6 \mu_2(s_2)x_2
\end{align*}$$
Before giving the structure of the designed observer for the system (3), we report in the next section a brief introduction to the invariant observers.

TABLE I: Model Parameters

<table>
<thead>
<tr>
<th>Acronym</th>
<th>Definition</th>
<th>Units</th>
</tr>
</thead>
<tbody>
<tr>
<td>$k_1$</td>
<td>Yield for $s_1$ degradation</td>
<td>Kg COD/Kg x$_1$</td>
</tr>
<tr>
<td>$k_2$</td>
<td>Yield for $s_2$ production</td>
<td>mol VFA/Kg x$_1$</td>
</tr>
<tr>
<td>$k_3$</td>
<td>Yield for $s_3$ consumption</td>
<td>mol VFA/Kg x$_2$</td>
</tr>
<tr>
<td>$k_0$</td>
<td>Yield for $e$ production</td>
<td>mol CH$_4$/Kg x$_2$</td>
</tr>
<tr>
<td>$\mu_{1,max}$</td>
<td>Maximum $x_1$ growth rate</td>
<td>1/day</td>
</tr>
<tr>
<td>$\mu_{2,max}$</td>
<td>Maximum $x_2$ growth rate</td>
<td>1/day</td>
</tr>
<tr>
<td>$k_{s1}$</td>
<td>Half saturation constant associated to $s_1$</td>
<td>Kg COD/m$^3$</td>
</tr>
<tr>
<td>$k_{s2}$</td>
<td>Half saturation constant associated to $s_2$</td>
<td>mol VFA/m$^3$</td>
</tr>
<tr>
<td>$k_{i}$</td>
<td>Inhibition constant associated to $s_2$</td>
<td>(mol VFA/m$^3$)$^{1/2}$</td>
</tr>
</tbody>
</table>

III. INVARIANT SYSTEM AND OBSERVER [5]

In the present work the invariance refers to the invariance under a group action. Hereafter, we give some references about this concept but for more comprehension the reader is referred to [4], [8] and for more details to [7].

Let consider the system (9) and let $G$ be a Lie group of transformations which acts on $X$ by $\varphi_g: X \rightarrow X \forall g \in G$. $\varphi_g$ is a diffeomorphism (at least $C^1$) on $X$ with $(\varphi_g)^{-1} = \varphi_g^{-1}$ and $\varphi_g \circ \varphi_{g_2} = \varphi_{g_1 \cdot g_2}$. Moreover, let’s note the action of the group $G$ on $U$ by $(\psi_g)_{g \in G}$ and on $Y$ by $(\rho_g)_{g \in G}$.

Definition 1. $G$ is a symmetry group of (9) if for every solution $(x(t), u(t))$ of (9) and $\forall g \in G, (\varphi_g(x(t)), \psi_g(u(t)))$ is also a solution.

Therefore, the system (9) is said to be invariant under $G$ if and only if $\forall g, x$ and $u$:

$$f(\varphi_g(x), \psi_g(u)) = D_{\varphi_g}(x)f(x, u)$$

where $D_{\varphi_g}$ is the Jacobian matrix of $\varphi_g(x)$.

After finding the group of transformation, one can write the following pre-observer for the system (9):

$$\dot{x} = F(\hat{x}, u, \hat{y})$$

if and only if $\forall x$ and $u$:

$$F(x, u, h(x, u)) = f(x, u)$$

Moreover, the pre-observer (5) is said to be invariant if and only if $\forall g, \hat{x}$ and $\hat{y}$:

$$F(\varphi_g(\hat{x}), \psi_g(\hat{y}), \rho_g(\hat{y})) = D_{\varphi_g}(\hat{x}(t))F(\hat{x}, u, \hat{y})$$

To design an invariant observer, we need invariant functions and invariant vector fields:

- A function defined on $X \subset R^n$ is invariant if and only if:
  
  $J(\varphi_g(x)) = J(x), \forall g$ and $x$.

- A vector field $\omega$ is invariant with respect to the action of $\varphi_g$ on $X$ if and only if:
  
  $\omega(\varphi_g(x)) = D_{\varphi_g}(x)\omega(x), \forall g$ and $x$.

Finally, it has been proven in [8] that the general form of an invariant pre-observer for the system (9) is given by:

$$\dot{x} = f(\hat{x}) + \sigma_1 J_s(\hat{x}) \omega(\hat{x})$$

with $J_s$ being an invariant function satisfying $J_s(\hat{x}, h(\hat{x}, u)) = 0$ and $\omega$ an invariant vector field. Moreover if (8) converges to (9) then it is called invariant observer.

IV. OBSERVER DESIGN

Before designing any kind of observer, one has to check first the observability of the system. To do so, we have used the rank criterium. Unfortunately, for lack of space, we have not included calculations in this note. However, we recall here below the used criterium [4]:

**Rank Criterium:** The non linear system:

$$\begin{align*}
\dot{x} &= f(x, u) \\
y &= h(x, u)
\end{align*}$$

where $x \in X \subset R^n$ is the state vector, $u \in U \subset R^m$ the input and $y \in Y \subset R^p$ is the measured output is observable if:

$$\text{rank} \left( dh, dL_fh, \ldots, dL_f^{n-1}h \right)^T = n$$

where $L_fh$ is the Lie derivative of $h$ along $f$.

$$L_fh = \sum_{i=1}^{n} f_i(x) \frac{\partial h}{\partial x_i}$$

and $dL_f^kh$ given by:

$$dL_f^kh = \left[ \frac{\partial L_f^kh}{\partial x_1}, \frac{\partial L_f^kh}{\partial x_2}, \ldots, \frac{\partial L_f^kh}{\partial x_n} \right]$$

For the system (3), $\text{rank} \left( dh, dL_fh, \ldots, dL_f^{n-1}h \right)^T = 4$, and thus the system is observable.

Now, after the system observability has been checked, we use the invariant functions and vector fields given in [4], to design the following invariant observer for system (3):

$$\begin{align*}
\dot{\hat{s}}_1 &= D(t)(s_{1in} - \hat{s}_1) - k_1 \mu_1(\hat{s}_1) \hat{x}_1 \\
&\quad + \sigma_1 (\ln \left( \frac{\hat{s}_1}{s_{1in}} \right) - \ln \left( \frac{\hat{s}_1}{\hat{s}_2} \right)) \\
\dot{\hat{s}}_2 &= (\mu_1(\hat{s}_1) - D(t)) \hat{x}_1 + a_2 \left( \ln \left( \frac{\hat{s}_1}{\hat{s}_2} \right) - \ln \left( \frac{\hat{s}_2}{s_{2in}} \right) \right) \\
&\quad + \sigma_1 (\ln \left( \frac{\hat{s}_2}{s_{2in}} \right) - \ln \left( \frac{\hat{s}_2}{\hat{s}_2} \right))
\end{align*}$$

with:

$$\begin{align*}
\mu_1(\hat{s}_1) &= \mu_{1,max} \frac{\hat{s}_1}{s_{1in} + k_1} \\
\mu_2(\hat{s}_2) &= \mu_{2,max} \frac{\hat{s}_2}{\hat{s}_2 + k_2 + \sigma_2 (\ln \left( \frac{\hat{s}_2}{s_{2in}} \right) - \ln \left( \frac{\hat{s}_2}{\hat{s}_2} \right))}
\end{align*}$$

and:

$$\hat{y} = k_6 \mu_2(\hat{s}_2) \hat{x}_2$$
Defining the errors: $e_1 = \ln(s_1) - \ln(\hat{s}_1), e_2 = \ln(x_1) - \ln(\hat{x}_1), e_3 = \ln(s_2) - \ln(\hat{s}_2), e_4 = \ln(x_2) - \ln(\hat{x}_2)$ and using Eqs. (3, 4, 10) and (11) we obtain the following:

$$\dot{e} = A(t)e + \Phi(t,e)$$  \hspace{1cm} (12)

with $e = [e_1, e_2, e_3, e_4]^T$, $A(t)$ the linear part of the error system:

$$A = \begin{pmatrix} -v_1 + v_2 & -v_3 & -a_1 & -a_1 \\ v_4 & 0 & -a_2 & -a_2 \\ -v_6 + v_7 & v_7 & A_{33} & -(a_3 + v_9) \\ 0 & 0 & -a_4 + v_11 - v_{12} & -a_4 \end{pmatrix}$$

where $A_{33} = -a_3 - v_5 - v_7 + v_8 + v_{10}$, and $\Phi(t,e) = [\Phi_1, \Phi_2, \Phi_3, \Phi_4]^T$ the non linear part:

$$\Phi_1 = -v_1(e^{e_1} - e_1 - 1) - v_2[f_1(e^{e_1} + e_1 - 1) + f_2(e^{e_2} + e_2 - 1) + a_1 \ln(g)]$$

$$\Phi_2 = -v_1[f_1(e^{e_1} + e_1 - 1) + f_2(e^{e_2} + e_2 - 1)e_1]$$

$$\Phi_3 = -v_5(e^{e_3} - e_3 - 1) + v_9[f_3(e^{e_3} + e_3 - 1) + f_4(e^{e_3} - 1)e_3 + f_5(e^{e_3 - 1}e_3) - v_10[f_3(e^{e_3} - 1)e_3 + 2f_5(e^{e_3 - 1})]$$

$$\Phi_4 = -v_{11}[f_3(e^{e_3} + e_3 - 1) + f_4(e^{e_3} - 1)e_3 + f_5(e^{e_3 - 1})e_3] + v_{12}[f_3(e^{e_3} + 2e_3 - 1) + f_4(e^{e_3 - 1})2e_3 + f_5(e^{e_3 - 1})2e_3]$$

where

$$\mu_{1,2} = 0.69, s_{1,2} = 15$$

Defining the errors:

$$\epsilon = [e_1, e_2, e_3, e_4]^T$$

where $A$ is the non linear part of the system (12), it can be easily seen that $\Phi(t,0) = 0$. Moreover, the function $\Phi(t,e)$ is continuous and differentiable. Thus, using the differential mean value theorem we can write:

$$\Phi(t,e) = \frac{\partial \Phi(t,z)}{\partial e} e$$

and moreover, we have:

$$||\Phi(t,e)|| \leq \left|\left| \frac{\partial \Phi(t,z)}{\partial e} \right| \right| e$$

Thus $\forall \epsilon > 0, \exists \delta_\epsilon > 0 : \forall e \leq \delta_\epsilon \Rightarrow ||\Phi(t,e)|| \leq \epsilon ||e||, \forall t \geq T$. Hence, the proof of the asymptotic stability of the origin for the system (12) has been completed.

V. Simulation Results

For simulation, we have taken $k_1 = 6.6$, $k_2 = 7.8$, $k_3 = 611.2$, $k_6 = 1139.2$, $k_s = 4.95, k_{s_2} = 9.28$, $k_{p_2} = 20$, $\mu_{1,2} = 1.2$, $\mu_{2,2} = 0.69, s_{1,2} = 15$ and $s_{2,2} = 80$. Furthermore, we have initialized the model at: $s_1(0) = 4, x_1(0) = 3.5, s_2(0) = 15$ and $x_2(0) = 0.3$. and the observer at: $s_1(0) = 5.5, x_1(0) = 3, s_2(0) = 13$ and $x_2(0) = 0.5$. Moreover, the simulation was carried out over 75 days with a varying input $D(t)$ as depicted in Fig (1). The obtained observer gain from the resolution of the LMI problem (Q > 0) is $K = [-15, -50, 120, 500]^T$.

The simulation results are plotted in figures (2, 3, 4) and (5). As it can be seen from the former figures, the designed observer is rapidly converging to the system state w.r.t the process dynamic. Moreover, we note that the addition of correction in the first two states ($s_1$ and $x_1$) allow the observer to be faster than the one proposed in [5].
VI. CONCLUSION

In this note, we have designed an invariant observer for the anaerobic digestion process with the use of an only one cheap and commonly done measurement at the industrial scale, which is the methane flow rate. The designed invariant observer has shown satisfactory behaviour and we target in the near future to evaluate its performance in the presence of noise in measurements, and finally use it for control in order to enhance the anaerobic digestion process.

APPENDIX

The following equations describe the dynamics of the system and its estimation. The equations are:

\[ v_1 = \frac{D(t) s_1}{t_1} \]
\[ v_2 = \frac{k_1 \mu_{1\text{max}} s_1 x_1}{(s_1 + k_1)^2} \]
\[ v_3 = \frac{k_1 \mu_{1\text{max}} x_1}{(s_1 + k_1)^2} \]
\[ v_4 = \frac{k_2 \mu_{2\text{max}} s_1 x_1}{(s_1 + k_1)^2} \]
\[ v_5 = \frac{D(t) s_2}{s_2} \]
\[ v_6 = \frac{k_2 \mu_{2\text{max}} s_1^2 x_1}{s_2 (s_1 + k_1)^2} \]
\[ v_7 = \frac{k_2 \mu_{2\text{max}} s_1 x_1}{s_2 (s_1 + k_1)^2} \]
\[ v_8 = \frac{D(t) x_1}{t_1} \]
\[ v_9 = \frac{k_3 \mu_{2\text{max}} s_2 x_2}{(s_2 + k_3)^2} \]
\[ v_{10} = \frac{2k_4 \mu_{2\text{max}} s_2^2 x_2}{(s_2 + k_4)^2} \]
\[ v_{11} = \frac{(s_2 + k_2 + \frac{s_2}{k_2})^2}{s_2 + k_2} \]
\[ v_{12} = \frac{2k_5 \mu_{2\text{max}} s_2}{(s_2 + k_5)^2} \]
\[ v_{13} = \frac{k_6 e^{-c_3} + k_6 + \frac{s_2}{k_6}}{s_2 + k_6} \]
\[ v_{14} = \frac{k_7 e^{-c_3} + k_7 + \frac{s_2}{k_7}}{s_2 + k_7} \]
\[ f_1 = \frac{s_1 + k_2}{s_1 e^{-c_1} + k_1} \]
\[ f_2 = \frac{s_1 e^{-c_1} + k_1}{s_1 + k_2} \]
\[ f_3 = \frac{s_2 e^{-c_3} + k_2 + \frac{s_2}{k_2}}{s_2 + k_2} \]
\[ f_4 = \frac{s_2 e^{-c_3} + k_2 + \frac{s_2}{k_2}}{s_2 + k_2} \]
\[ f_5 = \frac{k_2 (s_2 e^{-c_3} + k_2 + \frac{s_2}{k_2})}{s_2 + k_2} \]

REFERENCES